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*A.I. Bondarieva, V.Yu. Tobilko, Yu.M. Kholodko, B.Yu. Kornilovych, N.A. Zahorodniuk***EFFICIENT REMOVAL OF ARSENIC(V) FROM WATER USING IRON-CONTAINING NANOCOMPOSITES BASED ON KAOLINITE****National Technical University of Ukraine «Igor Sikorsky Kyiv Polytechnic Institute», Kyiv, Ukraine**

We studied the main physicochemical features of removing of arsenate from contaminated waters utilizing stabilized nanoscale iron. An inorganic kaolinite matrix was used for stabilization. The structure of adsorbents was studied using some physicochemical methods (X-ray powder diffraction and the low-temperature N<sub>2</sub> adsorption-desorption method). It was found that the efficiency of the removal of arsenic(V) ions depends on the weight ratio of iron nanopowder to kaolinite, whereas it does not depend on the pH of the water systems in a wide range. Kinetics data were analyzed using pseudo-first-order and pseudo-second-order models. It was stated that the removal of arsenic by iron-containing composites based on kaolinite occurs relatively rapid. The adsorption kinetic was appropriately described by the pseudo-second-order model, indicating the high affinity of arsenates with the surface of the iron-containing nanocomposite. The results demonstrated that the obtained materials have a much higher sorption capacity to As(V) ions than natural silicates. The Langmuir and Freundlich isotherm equations provided good fittings for the experimental sorption data. It was shown that the sorbents based on stabilized nanoscale iron effectively remove toxic arsenic ions from contaminated water.

**Keywords:** kaolinite, nanoscale zero-valent iron, nanocomposite sorbents, arsenic, water treatment, adsorption.

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**Introduction**

All living organisms are at risk from arsenic compounds, which are potentially toxic and carcinogenic. Arsenic (As) may enter the human body through both food (seafood, grain and meat) and the respiratory system (inhalation of air contaminated with gaseous waste after burning coal or industrial emissions). However, the most dangerous to human health are inorganic forms of arsenic, which enter the body through drinking water. Chronic exposure to As causes skin lesions, raises the risk of cancer and have a negative impact on the respiratory, nervous, and cardiovascular systems [1,2].

The problem of arsenic content in surface and groundwater is recognized in many countries on all continents and does not depend on the level of their economic development (Bangladesh, India, China, Argentina, Mexico, USA, Hungary, etc.). In some regions, its content in natural bodies of water reaches tens and hundreds of micrograms per 1 dm<sup>3</sup> [3]. Since the effects of arsenic on the human body are irreversible, only the prevention of its income in

drinking water can ensure the preservation of human health. According to the directive documents of the World Health Organization, the permissible concentration of arsenic in drinking water should not exceed 10 µg dm<sup>-3</sup>.

Pollution of groundwater with arsenic is basically caused by natural factors such as geochemical leaching and weathering processes from arsenic rocks [1,4]. As for surface waters, potential sources of contamination originate from effluents of industrial plants in non-ferrous extractive metallurgy, pigments, paints and printing industries, and as a result of agricultural activity, etc. [3,4].

In the environment, As exists in several oxidation states (-3, 0, +3, +5) that depend on dissolved oxygen concentrations, the redox potential and the pH of the aqueous system. The most common inorganic forms of As are arsenite forms (H<sub>3</sub>AsO<sub>3</sub><sup>0</sup> and H<sub>2</sub>AsO<sub>3</sub><sup>-</sup>), which are found in water bodies with anaerobic conditions, and arsenate forms (H<sub>2</sub>AsO<sub>4</sub><sup>-</sup> and HAsO<sub>4</sub><sup>2-</sup>), which are found in water bodies with oxidizing conditions [1,4].

In this context, there is a need to develop effective and safe technologies that would ensure the purification of water from arsenic to levels below the maximum contamination level. Various chemical and physicochemical methods are used to purify water from metal ion pollution. However, sorption technologies attract special attention among the recognized methods of water treatment from inorganic toxicants. This is because they enable a high level of heavy metal compounds removal from water [5].

Synthesis of sorbents based on food industry waste, agro-industrial complex waste, and natural raw materials such as zeolites and clays are receiving a lot of attention these days [6,7]. However, the majority of these materials are only efficient for treating natural and wastewater from pollutants that are cationic in nature, such as Cu(II), Zn(II), Ni(II), Co(II), Cd(II), Pb(II) [5,7].

Thus, the essential challenge is to obtain sorption materials for the efficient removal of inorganic anions (As(III), As(V), Cr(VI)) from water. Existent sorbents based on metal oxides and hydroxides (titanium, zirconium, cerium, aluminum and iron) are extremely successful in removing arsenic from water [8], but their major disadvantage is their high cost. Nanopowders based on nanoscale zero-valent metal (nZVM) such as iron, manganese, copper are of interest as an efficient material with high adsorption capacity against inorganic contaminants including arsenic [9]. Powders aggregation, fast oxidation and difficulty in separating nZVM from the treated solution pose substantial challenges to their application in environmental practice. To improve the efficiency of their usage in technological processes, highly reactive nZVM should be stabilized on the surface of organic or inorganic matrices. Activated carbon, silica gel, expanded clay, natural silicates and other materials are commonly used for this purpose [10].

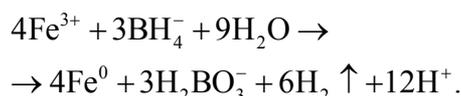
The development of sorbents based on natural clay minerals for water treatment from inorganic pollutants is promising. The structural features of clay minerals allow modifying their surface with various compounds and obtaining new functional materials with unique properties. For example, kaolinite is a common and inexpensive mineral with chemical, mechanical and thermal resistance [11]. In this regard, the relevance of the work is due to the need to develop new highly efficient sorbents based on natural clay mineral for the removal of anionic forms of toxicants from water.

The aim of the research is to study the main physicochemical features of the removal of arsenic

(V) from water using iron-containing nanocomposites based on kaolinite.

#### **Materials and methods**

The natural kaolin, the main rock-forming mineral of which is kaolinite (abbreviated as K in this study), from the Glukhovets deposit (Ukraine) was the object of this study. Before use, K was purified from impurities of quartz, feldspars, carbonates and other minerals by a sedimented method. The iron-containing nanocomposites (Fe<sup>0</sup>-K) was prepared following the methodology described elsewhere [12]. The kaolinite was first dissolved into deionized water and then, under stirring, added to iron (III) chloride hexahydrate solution with a certain concentration. The next dropwise addition of a solution of sodium borohydride NaBH<sub>4</sub> to a suspension of kaolinite for one hour resulted in a reduction of Fe<sup>3+</sup> ions. The reduction reaction is represented as follows:



After that, the obtained black suspension was stirred for another 1 hour to complete the redox reaction. The solid phase was then separated from the liquid phase by centrifugation. The samples were washed several times with ethyl alcohol and dried under a vacuum at a temperature of 60°C. The resulting precipitate was crushed and sieved to obtain a fraction ≤0.2 mm. As a result, we obtained 4 sorbents with different mass ratios of Fe<sup>0</sup>:K: 0.01:1; 0.05:1; 0.1:1 and 0.2:1.

Figure 1 shows a photo of the obtained sorbents, which demonstrates that their color varies depending on the amount of iron applied to the kaolinite surface. Moreover, the bigger Fe<sup>0</sup>, the blacker is the sample.

The efficacy of sorbent materials was evaluated using arsenic(V)-containing model solutions. An arsenic standard solution with a concentration of 1000 mg dm<sup>-3</sup> was used to this end. The ionic strength (I=0.01) was maintained using a 1 M NaCl solution.

To control the monomineralic character of K and determine the phase composition of the obtained iron-containing nanocomposites, X-ray powder diffraction (XRD) patterns were recorded on DRON-4-07 diffractometer in the range of 2 to 60° (2θ) using CuK<sub>α</sub> radiation.

The parameters of the porous structure were determined on evacuated samples by the low-temperature N<sub>2</sub> adsorption-desorption method (T=-196°C) (Quantachrome NOVA-2200e Surface Area and Pore Size Analyzer, USA). The results were processed using the ASiQwin™ V 3.0 software. The

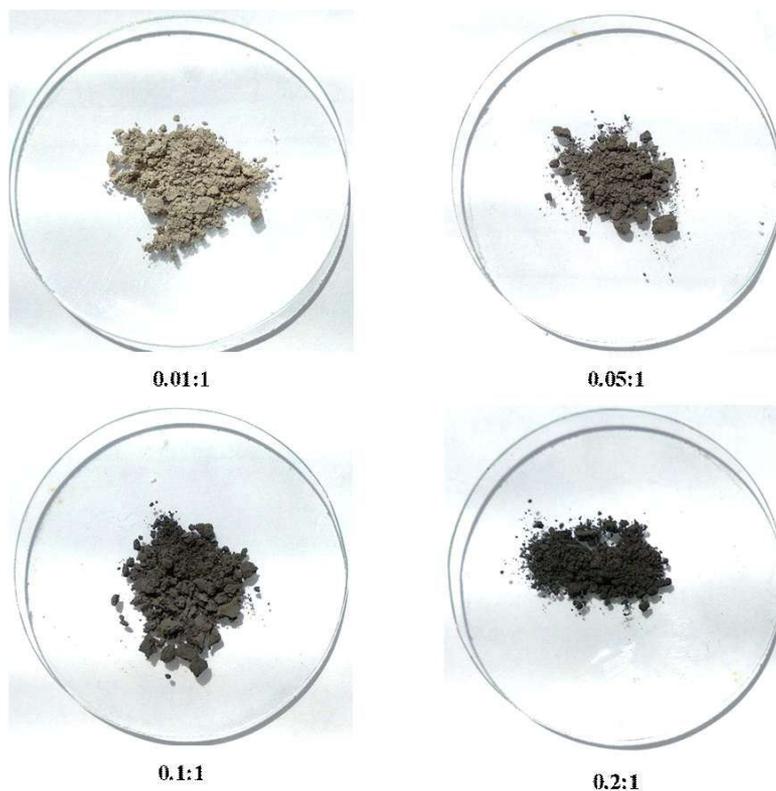


Fig. 1. Synthesized sorbents with different mass ratio Fe<sup>0</sup>:K

specific surface area ( $S_{\text{BET}}$ ,  $\text{m}^2 \text{g}^{-1}$ ) was measured by multipoint BET method (Brunauer-Emmett-Teller). The total pore volume ( $V_{\Sigma}$ ,  $\text{cm}^3 \text{g}^{-1}$ ) was calculated using the maximum adsorbed volume of nitrogen at a relative pressure  $p/p_0 \approx 0.99$ . The volume of micropores ( $V_{\mu}$ ,  $\text{cm}^3 \text{g}^{-1}$ ) was determined by the t-plot method, and their percentage was calculated using the following formula:

$$V_{\mu}, \% = \left( V_{\mu} / V_{\Sigma} \right) \cdot 100\%. \quad (1)$$

The efficiency of removing arsenic from water by using the obtained nanocomposites is dependent on many factors, including the mass ratio of Fe<sup>0</sup> to K, the sorbent dose, the pH of the water, the time of sorption equilibrium, and the initial concentration of As(V) in solution. All experiments were conducted by adding 0.1 g adsorbent to 50  $\text{cm}^3$  arsenic solutions.

To establish the optimal mass ratio of Fe<sup>0</sup>:K, which provides the maximum removal efficiency arsenic from water, we used a solution of As(V) with the concentration of 6  $\text{mg dm}^{-3}$  at pH=6.0.

In order to investigate the effect of pH on adsorption, the initial pH was varied from 3 to 8. The pH of the solutions was adjusted with 0.1 M solution NaOH and initial concentration of As(V) was 6  $\text{mg dm}^{-3}$ .

In the kinetic study, the initial model solutions with the concentration of 6  $\text{mg dm}^{-3}$  were stirred at different time intervals (10–240 min) in an orbital shaker at 190 rpm and the temperature of  $20 \pm 2^\circ\text{C}$ . Pseudo-first-order (PFO) and pseudo-second-order (PSO) models were used to describe the kinetic experimental results. The PFO and PSO rate equations can be respectively written as follows:

$$\ln(q_e - q_t) = \ln q_e - k_1 t, \quad (2)$$

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e}, \quad (3)$$

where  $q_e$  and  $q_t$  ( $\text{mg g}^{-1}$ ) are the adsorption capacity at equilibrium and at any time (min), respectively;  $k_1$  ( $\text{min}^{-1}$ ) and  $k_2$  ( $\text{g mg}^{-1} \text{min}^{-1}$ ) are the PFO and PSO rate constant, respectively.

The adsorption experiments were performed in the range of initial concentrations of 0.5–20  $\text{mg dm}^{-3}$  under static conditions at room temperature ( $20 \pm 2^\circ\text{C}$ ) and the ratio of solid and liquid phases S:L=1:500. The residual As(V) concentrations were determined by the inductively coupled plasma atomic emission spectroscopy (Thermo Scientific iCAP 7400 ICP-OES, USA).

The Langmuir (Eq. (4)) and Freundlich (Eq. (5)) isotherm equations were used to describe the experimental adsorption data of As(V) on the Fe<sup>0</sup>-K:

$$q_e = \frac{q_{\max} K_L C_e}{1 + K_L C_e}, \quad (4)$$

$$q_e = K_F C_e^{1/n}, \quad (5)$$

where  $q_e$  (mg g<sup>-1</sup>) is the equilibrium adsorption capacity,  $C_e$  (mg dm<sup>-3</sup>) denotes equilibrium concentration,  $q_{\max}$  (mg g<sup>-1</sup>) is the maximum adsorption capacity,  $K_L$  (dm<sup>3</sup> mg<sup>-1</sup>) denotes the Langmuir equilibrium constant, and  $K_F$  ((mg/g)(dm<sup>3</sup>/mg)<sup>1/n</sup>) and  $1/n$  are the Freundlich constants related to the adsorption capacity and adsorption intensity, respectively.

The removal efficiency (X, %) and adsorption capacity (q, mg g<sup>-1</sup>) of arsenate ions were estimated by Eq. (6) and Eq. (7), respectively:

$$X = \frac{C_0 - C_e}{C_0} \cdot 100\%, \quad (6)$$

$$q = \frac{(C_0 - C_e) \cdot V}{m}, \quad (7)$$

where  $C_0$  and  $C_e$  are the initial and equilibrium As(V) concentrations, respectively (mg dm<sup>-3</sup>),  $V$  is the solution volume (dm<sup>3</sup>), and  $m$  is the weight of adsorbent (g).

### Results and discussion

The X-ray diffraction patterns of K and Fe<sup>0</sup>-K (0.2:1) are shown in Fig. 2. According to the XRD pattern of K (Fig. 2,a), the diffraction peaks at  $2\theta=12^\circ$  (0.715 nm),  $20^\circ$  (0.434 nm),  $25^\circ$  (0.358 nm) and  $38^\circ$  (0.238 nm) correspond to the kaolinite phase that agrees with ICDD database PDF File No. 01-078-2110. The presence of characteristic reflections at  $2\theta=21^\circ$  (0.426 nm) and  $27^\circ$  (0.334 nm) confirms the existence of quartz traces (PDF File No. 01-083-2472). The existence of a modifying layer of iron compounds consisting of the crystalline phase  $\alpha$ -Fe at  $2\theta=45^\circ$  (0.198 nm) (PDF File No. 01-076-6588) and small signals of iron oxide FeO and iron oxyhydroxides FeOOH on the surface of the iron-containing sample are shown by XRD (Fig. 2,b).

According to the modified de Boer classification, the nitrogen sorption isotherms (Fig. 3) on the investigated materials are of type II (b) isotherms [11]. The shape of the isotherms is typical of non-porous sorbents and indicates that the samples have a mainly macroporous structure, with micro- and mesopores being practically or entirely absent. The narrow hysteresis loop of type H3 on isotherms is caused by capillary condensation in kaolinite structural aggregates between weakly linked flat elementary packages of the mineral. Furthermore, narrow hysteresis indicates the presence of fine macropores. The calculated parameters of the samples porous structure are shown in Table 1.

The BET surface area of Fe<sup>0</sup>-K is insignificantly reduced following surface modification K. This decrease is due to the Fe<sup>0</sup> aggregation processes of tiny clay particles and almost full closure of

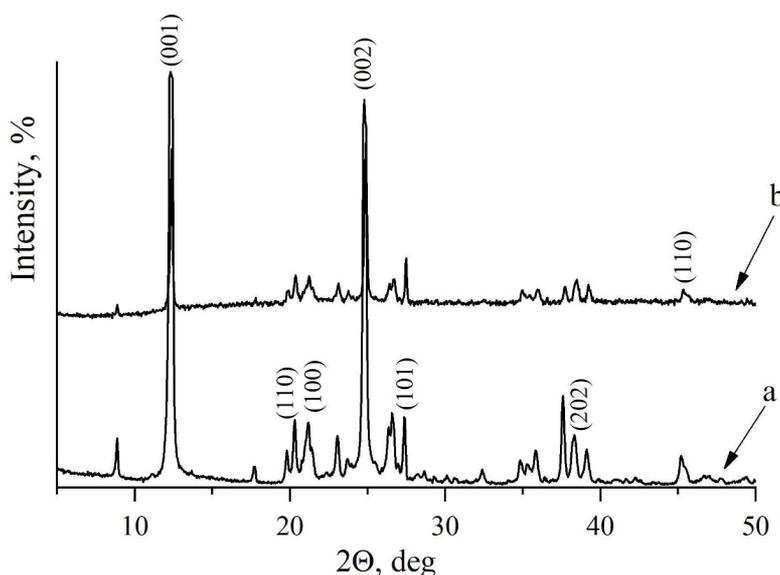


Fig. 2. X-ray powder diffraction patterns of pure (a) and modified (b) kaolinite

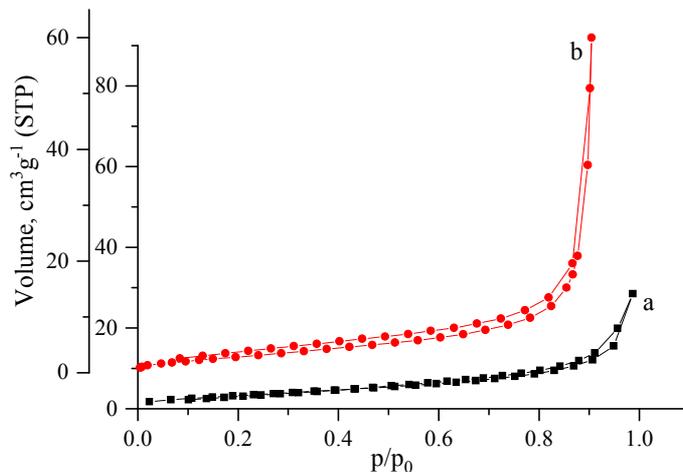


Fig. 3. Adsorption-desorption isotherms of N<sub>2</sub> of pure (a) and modified (b) kaolinite

micropores with Fe<sup>0</sup> films, resulting in the limited access of nitrogen molecules to these pores.

Table 1  
Characteristics of the porous structure of the K and Fe<sup>0</sup>-K samples (0.2:1)

Sample	S <sub>BET</sub> , m <sup>2</sup> g <sup>-1</sup>	V <sub>Σ</sub> , cm <sup>3</sup> g <sup>-1</sup>	V <sub>μ</sub> , cm <sup>3</sup> g <sup>-1</sup>	V <sub>μ</sub> , %
K	12.84	0.0423	0.0027	6.38
Fe <sup>0</sup> -K	11.72	0.0930	0.0029	3.12

Figure 4 illustrates the dependence of the removal efficiency from arsenate ions on the amount of Fe<sup>0</sup> applied to the surface of kaolinite. According to the findings, an increase in the concentration of nanoscale iron on the surface of kaolinite improves composite adsorption ability. The maximum removal efficiency is 97.74% for a sample with a mass ratio of Fe<sup>0</sup>:K=0.2:1. Thus, this sorbent was chosen for further study.

The obtained experimental data indicate that

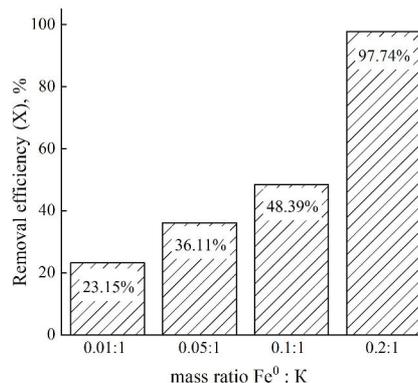


Fig. 4. Diagram of the dependence of the removal efficiency of As(V) on the content of Fe<sup>0</sup> on the surface of kaolinite

the pH value does not affect the process of As(V) adsorption for Fe<sup>0</sup>-K across a wide range. This is due to the electrostatic interaction between the

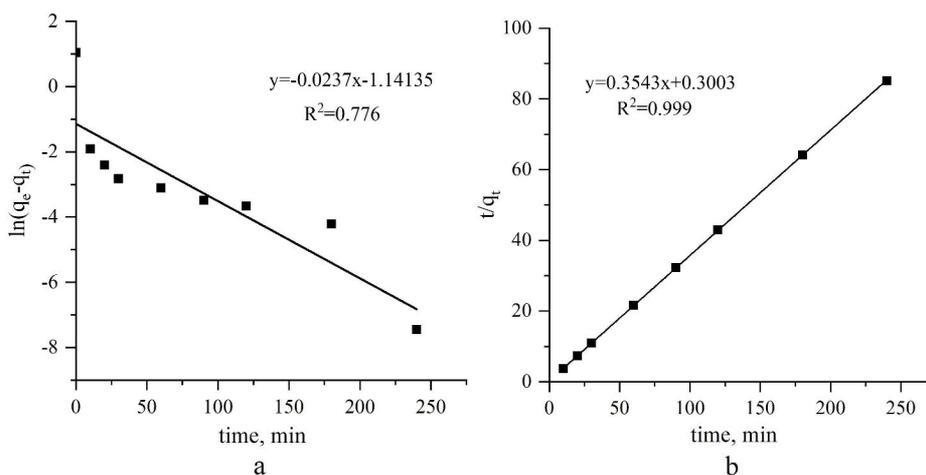


Fig. 5. Kinetics of arsenic (V) adsorption on Fe<sup>0</sup>-K composite plotted in the coordinates of the pseudo-first-order model (a) and the pseudo-second-order model (b)

Table 2

Kinetic parameters of As(V) adsorption on Fe<sup>0</sup>-K (C<sub>0</sub>=6 mg dm<sup>-3</sup>, T=293 K, pH=6.2)

Kinetic models	Parameters			
	Pseudo-first-order	q <sub>e, exp.</sub> (mg g <sup>-1</sup> )	q <sub>e, cal.</sub> (mg g <sup>-1</sup> )	k <sub>1</sub> , min <sup>-1</sup>
	2.819	0.320	0.0237	0.776
Pseudo-second-order	q <sub>e, exp.</sub> (mg g <sup>-1</sup> )	q <sub>e, cal.</sub> (mg g <sup>-1</sup> )	k <sub>2</sub> , g mg <sup>-1</sup> min <sup>-1</sup>	R <sup>2</sup>
	2.819	2.82	0.415	0.999

positively charged surface of nanoscale zero-valent iron particles and the negatively charged form of H<sub>2</sub>AsO<sub>4</sub><sup>-</sup> in the pH range of 3–7 [13].

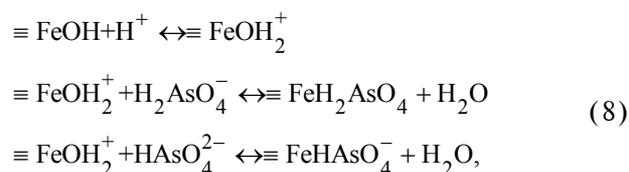
The kinetic experimental data shows a relatively intense rate of As(V) adsorption on iron-containing nanocomposite based on kaolinite. Rapid adsorption observes during the first 30 min of contact time. Then, metal adsorption is increasing somewhat until it reached equilibrium. It took around 60 minutes of contact time to get this condition.

PFO and PSO kinetic models of arsenic sorption on Fe<sup>0</sup>-K in the linear forms are shown in Fig. 5. The calculated parameters of the kinetic models are summarized in Table 2.

Analysis of the regression correlation coefficient (R<sup>2</sup>) shows that the kinetic dependence fits the PSO model (R<sup>2</sup>>0.99) better than the PFO model (R<sup>2</sup>>0.77). This indicates a high affinity between arsenate ions and sorbent. Furthermore, the theoretical value of sorption (q<sub>e, cal.</sub>) at equilibrium is extremely near the experimental value (q<sub>e, exp.</sub>).

Since the main activity centers of the synthesized material are provided in the form of nanoscale zero-valent iron particles with a «core-shell» structure, the sorption process begins on the

surface of the sorbent:



After all external sorption centers have been filled with adsorbate, arsenate ions can enter the pores of the material where internal adsorption occurs. As the concentration of As(V) in the solution diminishes over time, so does the diffusion rate, and an equilibrium condition is attained [14].

Isotherms of sorption of As(V) on the natural and modified samples of kaolinite at pH 6.0 are shown in Fig. 6. The results demonstrate that the sorbent with the deposited layer of Fe<sup>0</sup> has a considerably higher sorption capacity towards arsenate ions than the native material. Thus, the maximum adsorption capacity of arsenate ions on Fe<sup>0</sup>-K is 6.2 mg g<sup>-1</sup>, whereas it is only 0.1 mg g<sup>-1</sup> on K. The calculated coefficients in Langmuir and Freundlich equations are shown in Table 3.

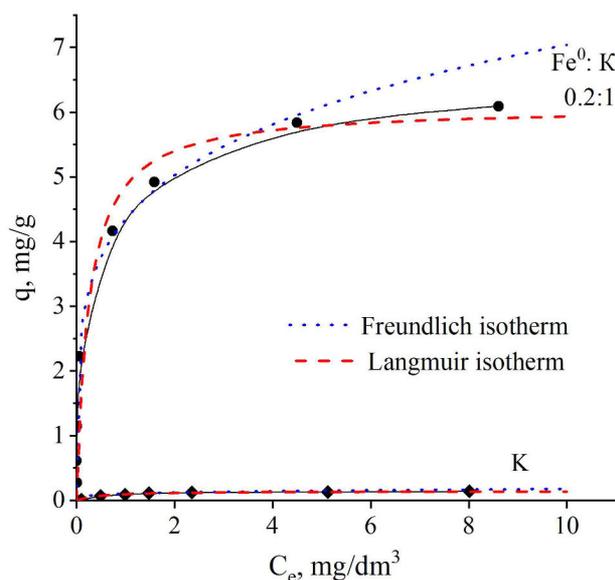


Fig. 6. Sorption isotherms of As(V) ions on natural kaolinite and iron-containing nanocomposite

Table 3  
Parameters of Langmuir and Freundlich adsorption isotherm equations

Sample	Langmuir constants			Freundlich constants		
	$q_{\max}$ , $\text{mg g}^{-1}$	$K_L$ , $\text{mg dm}^{-3}$	$R^2$	1/n	$K_F$	$R^2$
Fe <sup>0</sup> -K (0.2:1)	6.089	3.971	0.996	0.222	4.33	0.995
K	0.143	1.970	0.998	0.268	0.090	0.916

The obtained data show that the adsorption of As(V) on modified kaolinite is well described by both the Freundlich and Langmuir equations, which is indicated by close to 1 correlation coefficient ( $R^2 > 0.99$ ).

### Conclusions

Iron-containing nanocomposites based on the clay mineral kaolinite were prepared. It was established that the stabilization of nanoscale zero-valent iron on the inorganic matrix avoids aggregation and rapid oxidation of the nanopowder and promotes better separation of the spent sorbent from the liquid phase. It was demonstrated that the produced materials have substantially higher As(V) adsorption capacity than natural kaolinite. It was found that the efficiency of the removal of arsenic(V) ions depends on the mass ratio of nanopowder of iron and kaolinite. Thus, a sample with a mass ratio of nanoscale zero-valent iron to kaolinite of 0.2:1 is the most effective. The pH of water systems has no effect on the removal effectiveness of arsenate ions by obtained nanocomposite in the pH range of 3–7. The adsorption kinetic is appropriately described by the pseudo-second-order model. The iron-containing nanocomposites based on kaolinite can be used for the water treatment from arsenic and other anionic toxicants.

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## ЕФЕКТИВНЕ ВИДАЛЕННЯ АРСЕНУ(V) ІЗ ВОДИ З ВИКОРИСТАННЯМ ЗАЛІЗОВМІСНИХ НАНОКОМПЗИТІВ НА ОСНОВІ КАОЛІНІТУ

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В даній роботі встановлено основні фізико-хімічні особливості видалення арсенатів із забруднених вод з використанням стабілізованого нанорозмірного заліза. Стабілізацію виконували на неорганічній матриці каолініту. За допомогою фізико-хімічних методів дослідження (рентгенофазовий аналіз, метод низькотемпературної адсорбції-десорбції азоту) вивчено структуру адсорбентів. Показано, що ефективність вилучення арсенат-іонів залежить від масового співвідношення нанопорошку заліза і каолініту, а ступінь очищення вод не залежить від рН водного середовища в широкому діапазоні. Виконано аналіз процесів кінетики сорбції арсенат-іонів зразками стабілізованого нанорозмірного заліза за допомогою кінетичних моделей адсорбції псевдо-першого та псевдо-другого порядків. Встановлено, що вилучення арсену залізозмісними композитами на основі каолініту відбувається досить швидко. Кінетична залежність сорбції As(V) одержаними залізозмісними матеріалами краще описується моделлю псевдо-другого порядку, що вказує на високу спорідненість арсенатів з поверхнею залізозмісного нанокompозиту. Встановлено, що одержані матеріали проявляють значно кращу сорбційну здатність щодо іонів арсену(V) у порівнянні з природними силікатами. Ізотерми сорбції арсену(V) модифікованим каолінітом добре описуються і рівнянням Фрейндліха, і Ленгмюра. Показано, що сорбенти на основі стабілізованого нанорозмірного заліза ефективно вилучають токсичні іони арсену із забруднених вод.

**Ключові слова:** каолініт, нанорозмірне нульвалентне залізо, нанокompозитні сорбенти, арсен, очищення води, адсорбція.

## EFFICIENT REMOVAL OF ARSENIC(V) FROM WATER USING IRON-CONTAINING NANOCOMPOSITES BASED ON KAOLINITE

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We studied the main physicochemical features of removing of arsenate from contaminated waters utilizing stabilized nanoscale iron. An inorganic kaolinite matrix was used for stabilization. The structure of adsorbents was studied using some physicochemical methods (X-ray powder diffraction and the low-temperature N<sub>2</sub> adsorption-desorption method). It was found that the efficiency of the removal of arsenic(V) ions depends on the weight ratio of iron nanopowder to kaolinite, whereas it does not depend on the pH of the water systems in a wide range. Kinetics data were analyzed using pseudo-first-order and pseudo-second-order models. It was stated that the removal of arsenic by iron-containing composites based on kaolinite occurs relatively rapid. The adsorption kinetic was appropriately described by the pseudo-second-order model, indicating the high affinity of arsenates with the surface of the iron-containing nanocomposite. The results demonstrated that the obtained materials have a much higher sorption capacity to As(V) ions than natural silicates. The Langmuir and Freundlich isotherm equations provided good fittings for the experimental sorption data. It was shown that the

sorbents based on stabilized nanoscale iron effectively remove toxic arsenic ions from contaminated water.

**Keywords:** kaolinite; nanoscale zero-valent iron; nanocomposite sorbents; arsenic; water treatment; adsorption.

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