

# Optimization of Sono-Electrocoagulation Process for the Removal of Dye Using Central Composite Design

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## ABSTRACT

Sono-electrocoagulation process was successfully applied for the removal of RR120 (Reactive Red 120) in the presence of activated carbon. For this purpose, the process variables were optimized using CCD (Central Composite Design). The operational parameters of the technology were the amount of activated charcoal (0.2-2.0g), amount of NaCl electrolyte (1-10g), sonication time (30-120 min) and RR120 dye concentration (40-120 mg/L), respectively. Consequently, the 100% dye removal was determined at the optimal conditions for the process obtained by CCD. In addition, the sonication time, amount of adsorbent and dye concentrations were found the significant process factors. Furthermore, the effects of other parameters like the electric current, current efficiency, amount of NaCl, temperature and formation of coagulants were also studied in the dye removal process, separately. The FTIR (Fourier Transfer Infrared) spectrums were monitored to identify the classes of functional groups present in the dye molecule before and after the treatment. Therefore, the sono-electrocoagulation process was proved an effective technique for purifying simulated wastewater containing RR120 dye.

**Key Words:** Sono-Electrocoagulation, Reactive Red120, Central Composite Design, Activated Carbon, Fourier Transfer Infrared.

## 1. INTRODUCTION

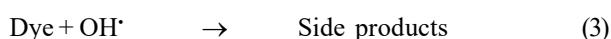
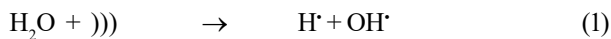
Water is essential for the existence of life on the earth. It provides medium to all biochemical activities in the living organisms. It is used for domestic, agriculture and industries. Moreover, it has the large consumption in industries. A large volume of wastewater is discharged off from industries. Due to improper treatment of wastewaters, contaminants are being added in water natural resources. Therefore, water pollution has become a major problem in the world. In the past, different methods

have been adopted to treat wastewater to reduce water pollution. Different treatment methods include chemical coagulation, adsorption, chemical-oxidation, photolysis, photo-catalysis, electro-photocatalysis [1-2]. Among different treatment processes, the EC (Electrocoagulation) process has also been used to treat wastewater. Furthermore, It has been applied to remove oils, colorants, metals, halides, etc. [3-4]. In the recent years, the EC process has been studied by researchers for the treatment of simulated and real wastewater of colors [5-

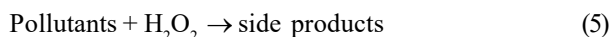
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6]. The EC process requires proper conductivity of the system and less energy consumption [7]. The process has been proved to be a precised, critical and less time-consuming technique [8-9]. Now-a-days, the applications of ultrasonic process are gaining importance by many researchers for the treatment of raw water [10-11]. The ultrasonic waves generated with ultrasonicator are transmitted in the liquid medium. As a result, air cavities are formed: cause molecular disintegrations. Additionally, they also generate ions and radicals in the solution [12-13]. Indeed, the sonic field increases the rate of formation of coagulants, during the EC method [14-15]. By employing the ultrasonic waves with the EC process, the OH<sup>•</sup> radicals are generated in wastewater which favor the subsequent oxidation of pollutants. Furthermore, many researchers have studied that the generation of hydroxyl radicals follow the first order kinetics [16]. Moreover, oxygen evolution occurs at the aluminium anode [17-18]. The mechanism of water sonolysis is represented as follows:



Water molecules undergo decomposition reaction in the presence of sonic field. It was firstly identified by Weiss, while, the synthesis of hydrogen peroxide was analyzed by Fitzgerald [19]. The generation of hydrogen peroxide, additionally, helps the EC process in contaminants removal from wastewater [20].



The diffusion-controlled processes are involved for the interactions of electrons containing water molecules, hydrogen atoms and OH<sup>•</sup> radicals. However, the chemical

species like hydrated electrons and hydrogen atoms have less reaction probability with the dye molecules. Because, oxygen molecule acts as scavenger of hydrogen radicals and hydrated electrons. Consequently, these species are transformed into peroxide and superoxide radicals. Because, the reduction potential of RR120 dye azo group is more negative about -0.35 V (versus NHE) as compared to the reduction potentials of perhydroxyl (-0.33V) and superoxide (-0.037V) radicals. Therefore, perhydroxyl and superoxide radicals jointly couldn't reduce the azo group of RR120 at pH 7. Because, azo group is strong reducing agent. Hence, it does not undergo reduction process. Furthermore, Reactive dyes are consumed at large industrial scale [21]. So, the removal of an anionic dye (RR120) has been studied. It has the potential risk to the bio-ecosystem because of its poor biodegradability [22-23]. Additionally, optimization of experimental variables on EC was analyzed by RSM (Response Surface Methodology) [24]. The purpose of RSM is to perform fewer experiment runs to optimize the operational parameters. Factors such as the amount of adsorbent (activated carbon) (g), electrolyte dosage of NaCl (g), sonication time (min) and dye concentration (mg/L) were selected as the operational parameters. Whereas, the removal of dye from simulated wastewater was analyzed as a response [25].

## 2. MATERIALS AND METHOD

### 2.1 Experiment Section

#### 2.1.1 Apparatus and Instruments

The sono-electrocoagulation process was performed at laboratory scale. Lab setup is shown in Fig. 1. The experimental runs of the sono-electrocoagulation were performed in a 1000 mL cylindrical glass reactor and placed in water bath sonicator [Elmasonic E 30 H]. Aluminium and graphite electrodes were selected as the anode and cathode and they were in rod shape. All the experiments

were attempted at 34°C. The weight of substances was measured by the Adventure Oahu's digital weighing balance model AR2140. While, the pH and temperature of dye solutions were measured with a Portable pH/EC/TDS/Temperature HANNA, HI9811-5. The absorbance was measured with UV/VIS Spectrophotometer T80 (PG Instruments LTD). Whereas, FTIR model NICOLET 67000 was used to obtain spectrums of pure RR120 dye and its sludge formed by the EC treatment.

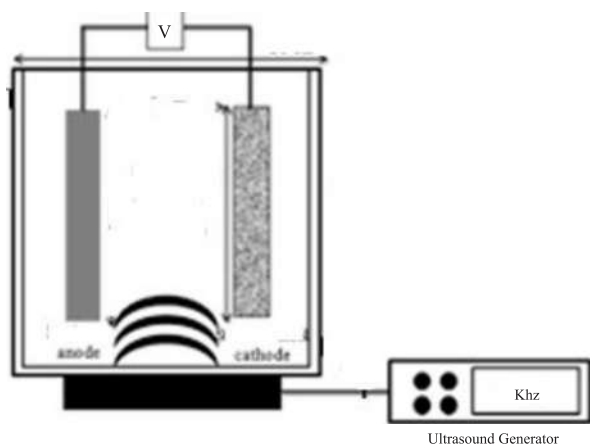


FIG. 1. THE SONO-ELECTROCOAGULATION SETUP FOR RR120 DYE REMOVAL

## 2.1.2 Reagents and Material

The physiochemical properties of RR120 are shown in Table 1.

## 2.1.3 Experimental Procedure

A stock solution of artificial RR120 dye was prepared. The diluted solutions were prepared between 30-1200mg/L from the stock solution. The number of experimental runs were determined by the Minitab 17 software. At the beginning of each trial, a fresh solution of RR120 dye, activated carbon(s) and NaCl(s) according to the experimental runs of the EC process was transferred into a 1000 mL glass reactor. After that, the EC reactor was turned on in water bath Sonicator (Elmasonic E 30H) for desired ultrasonic intervals as designed by the Minitab 17 software. The sono-electrocoagulation reactor was connected to a digital DC power supply (Yaxun 1502DD; 15V, 2A). The amplitude was set at 100%. After the specified interval of the sono-electrocoagulation process the samples were ejected and after filtration they were

TABLE 1. PROPERTIES OF REACTIVE RED 120 DYE

Dye	Reactive Red 120
Chemical Structure	
CAS No.	61951-82-4
Chemical Name	Reactive Red 120
Synonyms:	Reactive Red HE7B
Molecular Formula	C44H24Cl2N14O20S6Na6
Formula Weight	1469.98
Properties and Applications	It is soluble in water. It is used for colorful blue-ray red color, iron particles change this color into slightly yellow and copper ions successively in turn light blue. Furthermore, primarily it is used for cotton or viscose fiber volume dyes and disseminated. It conjointly appropriate for direct printing and also suitable for polyester/cotton, polyester/stick blended coloring.
max	532 nm
CB Number	CB0402020

analyzed at  $\lambda_{\max}$  of 532 nm with T80 UV-VIS Spectrophotometer. Furthermore, the electrodes were cleaned with 5%  $H_2SO_4$  (w/v) solutions and the EC reactor was also washed by utilizing 2% HCl solutions.

## 2.2 Response Surface Methodology

### 2.2.1 Central Composite Design

The amount of adsorbent (Activated Carbon), electrolyte quantity (NaCl), sonication time and dye concentrations (RR120) were optimized for the removal of dye using CCD. The % removal of dye was considered to be dependent on the amount of adsorbent (Activated Carbon), the electrolyte quantity (NaCl), sonication time and dye concentration (RR120).

$$y = \beta_0 + \sum_{i=1}^4 \beta_i x_i + \sum_{i=1}^4 \sum_{j=1}^4 \beta_{ij} x_i x_j + \sum_{i=1}^4 \beta_{11} x_i^2 \quad (6)$$

The symbols  $X_i, X_j$  are showing the independent variables,  $\beta_0$  is the intercept of the model. The linear coefficient is  $\beta_i$ , and the quadratic coefficients are  $\beta_{ij}, \beta_{ii}$ .

### 2.2.2 Statistics Modeling

The Minitab 17 Software was used to design the experimental runs. It was also employed for calculating ANOVA (Analysis of Variance), multiple regression analysis, full interaction plots and the main interaction effects. Furthermore, the Sigma Plot 12 software was used to draw the response surface plots in order to study the effects of two variables at a time on the response.

## 3. RESULTS AND DISCUSSION

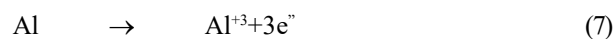
### 3.1 Mechanism of the EC Process

The mechanisms of the EC process are not so simple. It needs further study to illustrate the EC mechanisms for

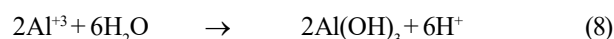
the removal of pollutants from wastewater [26]. The mechanism of the process is represented as follows:

Mechanism

At Anode:



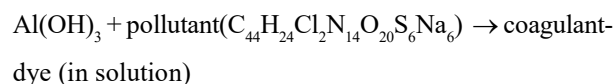
Bulk of solution:



At Cathode :



Over all reaction:



The removal potency of the dye depends on the amount of  $Al(OH)_3$  generated by the oxidation of the metal electrode. Consequently, the high removal efficiency was observed for the longer time period and the maximum electric potentials. The pH of the system also favors the synchronous formation of  $Al(OH)_3$ . While,  $Al^{3+}$  and  $OH^-$  ions are generated by the electrode reactions as shown in Equation (7-9). After that, they form various aluminium species such as  $Al(OH)^{2+}$ ,  $Al(OH)_2^+$ ,  $Al(OH)_2^{4+}$ ,  $Al(OH)_4$  and polymeric species such as  $Al_6(OH)^{3+}$ ,  $Al_7(OH)_{17}^{4+}$ ,  $Al(OH)^{4+}$ ,  $Al_8(OH)_{20}^{4+}$ ,  $Al_{13}O_4(OH)_{24}^{7+}$ ,  $Al_{13}(OH)_{34}^{5+}$ , finally, which are transformed into  $Al(OH)_3$  chemical species according to the complex precipitation kinetics. Numerous interaction mechanisms are possible between the dye molecules and hydrolysis products and their rates depend on the pH of the EC system and sorts of particles present in the

system. The two major interface mechanisms were being considered in the recent years. The precipitation and adsorption processes, being proposed at separate pH data. Flocculation process occurs in a less acidic media and elucidated as precipitation. While, the adsorption process is followed at high pH. At high basic media pH > 9,  $\text{Al}(\text{OH})_4^-$  ions are additionally present in the system.  $\text{Al}(\text{OH})_3$  has reactive surface sites naturally which favor fast adsorption of solvent impurities and accumulation of colloidal particles [27]. Furthermore, Al precipitates are generated at high pH >7.

### 3.2 FTIR Analysis of RR120 Dye

Fig. 2(a-b) represent the FTIR spectrum of RR120 dye before and after the sono-electrocoagulation treatment. The characteristic peak which represents the Nitrogen-Hydrogen stretching present outside the benzene ring appeared near to  $3500\text{cm}^{-1}$ . While the peak which is showing the CH (Carbon-Hydrogen) distortion in  $\text{CH}_3$  group appeared at  $1365\text{cm}^{-1}$ . The peak at  $1174\text{cm}^{-1}$  is owing to CH stretching in benzene ring. The peaks at  $3000\text{-}3100\text{cm}^{-1}$  represent at the stretching of CH in benzene. Moreover, between  $1400\text{-}1600\text{cm}^{-1}$  represent C=C stretching in benzene ring. The low intensity absorption was observed between  $4000\text{-}2000\text{cm}^{-1}$ . The number of peaks was additionally reduced of the dye once its surface was attached by the coagulants. The percent transmittance decreased at  $3446\text{cm}^{-1}$  after the sono-electrocoagulation treatment of RR120 dye simulated effluent. The broader peak at  $3446\text{cm}^{-1}$  is showing that -OH groups have been increased in the sludge. Which is further confirmed from its high absorption in the spectrum.

### 3.3 The Sono-Electrocoagulation Process for the Removal of RR 120 Dye

#### 3.3.1 RSM to Optimize the Operative Parameters

Optimization of the sono-electrocoagulation process OOP (Optimize Operating Parameters) was carried out. The amount of adsorbent (activated carbon) was varied from (0.2-2 g), whereas the amount of electrolyte (NaCl) was maintained as (1.0-10g). The sonication time at the lowest level of 30 min to the highest level of 120 min was retained. The concentration of RR120 dye with the lowest level of 30 mg/L to the highest level of 120mg/L was selected.

The RSM model is represented in Equation (10):

$$\begin{aligned} \% \text{ Color Removal} = & 103.7 + 10.8 A + 0.83 B + 0.232 C - 0.659 \\ & D - 2.33 AA - 0.093 BB - 0.00340 CC - 0.00024 DD - 0.062 \\ & AB - 0.0926 AC + 0.0625 AD + 0.0062 BC + 0.0014 BD + \\ & 0.00653 CD \end{aligned} \quad (10)$$

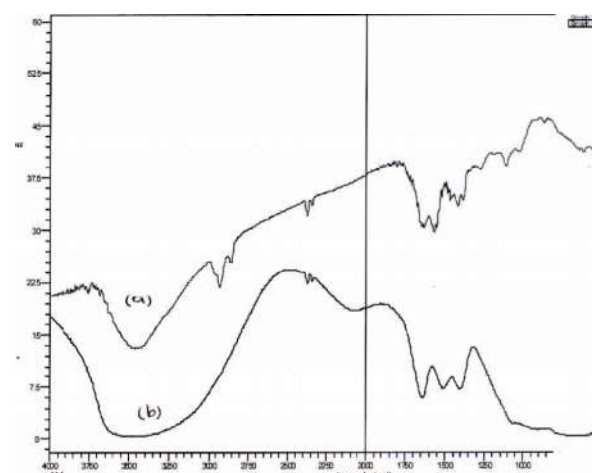


FIG. 2. THE FTIR SPECTRUM OF (a) A PURE RR 120 DYE (b) THE FTIR SPECTRUM OF RR 120 DYE AFTER THE SONO-EC TREATMENT

While A, B, C and D are representing the coded variables such as the amount of adsorbent (Activated carbon), the quantity of electrolyte (NaCl), sonication time and RR120 dye concentrations, respectively. The optimum parameters were evaluated by the RSM graphs as delineated in Fig. 3(a-c).

The sono-electrocoagulation process is enhanced gradually by increasing the sonication time and amount of electrolyte. The regular residuals for the % dye removal and frequency are represented in Fig. 4(a).

The Fig. 4(a) is showing that the utmost residuals lie within the intervals between -5 and 5. A normal probability graph for the RR120 dye removal is shown in Fig. 4(b). It allocates that the points are symmetrically around the central line. The data sets are showing a linear relation and that is confirmed by the experimental design. Additionally, the CCD has the significant importance. It is cleared from Fig. 4(b) that there is no significant outlier relative to a normal distribution is noticed within the plots. By the examination of variance, it is generally more viable (and straightforward) to perform this with the residuals. The residuals and the observation order of the data are

shown in Fig. 4(c). The data points are shown on the x-axis. While Experiments No. 4, 11, 29 are providing the large residuals. The significance and non-significance of variables can be identified by a Pareto Chart as displayed in Fig. 5.

The effective parameters of the sono-electrocoagulation process for the removal of RR120 dye are the sonication time, dye concentration and amount of adsorbent. Other significant factors include the amount of adsorbent (activated carbon), and combined effects of other respective factors (CD) and C<sup>2</sup>.

Table 2 represents the model outline of the experimental design found by the Minitab 17 Software for sono-electrocoagulation method for the removal of RR120. The R<sup>2</sup> value 0.8226 is representing the importance of the model. Whereas, its adjusted value is found to be 0.6673. When model does not show worth, the lack of fit shows significance. The p-value for the lack of fit is found to be >0.05 for RR120 removal: shows that the F-statistic is insignificant, suggesting the consequential model relationship between the elemental factors and process response. The adequacy of the

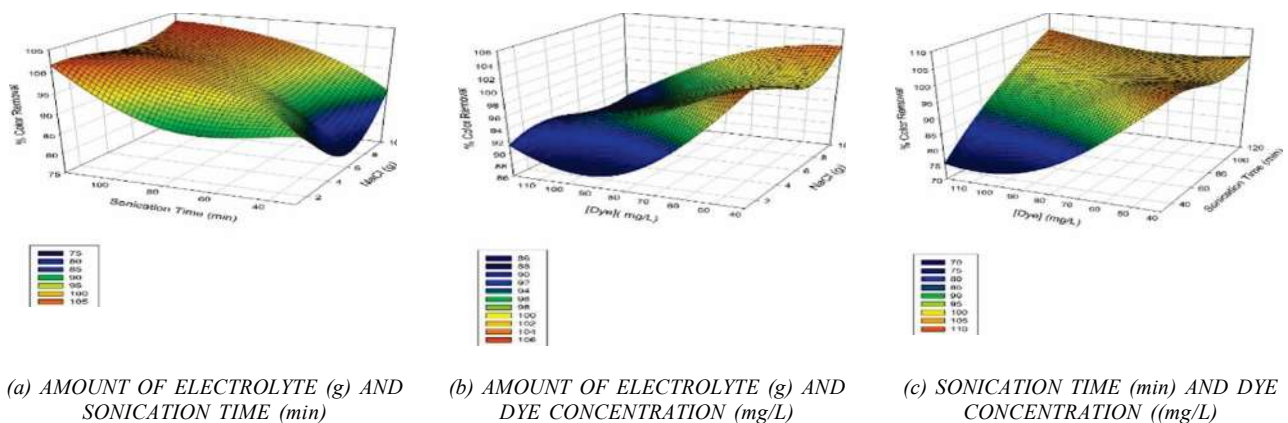


FIG. 3. RESPONSE SURFACE DIAGRAMS AS A FUNCTION OF % DYE REMOVAL

regression model for explaining the experimental data at 95% confidence level is tested by the ANOVA. It includes some statistic factors such as lack of fit,  $R^2$ , and adjusted  $R^2$ . The ANOVA results are shown in Table 3, representing that the model is extremely impertinent, as the P-value for the model is 0.001 (P-value < 0.05). The higher  $R^2$  value is indicated that the applied model offers conventional estimated response of the system. The significance of “lack of fit” with (P-value > 0.05) is indicated that the factors are satisfactorily fitted the data of target response. All relations within the regression model aren't equally important. The significance of each term is analyzed by the student's t-test and P-values, data is represented in Table 4. The t-

test represents the quantitative relation of the estimable parameters and their impacts to the computable parameter of variance. The t-test ( $t_{cal} < t_{tab}$ ) and smaller P-values of the coefficients declare the additional significance. Table 3 represents the analysis of variance ANOVA and P-values. It is cleared from the data that some P-values are reduced compared to the confidence level (0.05). It represents the appropriateness and importance of the processes. The terms B, AB, AC, AD, BC, BD are not found to be comparatively essential for the elimination of the RR120 dye. The factor sonication time (C), dye concentration (D) and amount of adsorbent are the foremost noteworthy dynamic which are agreed by the Pareto chart too.

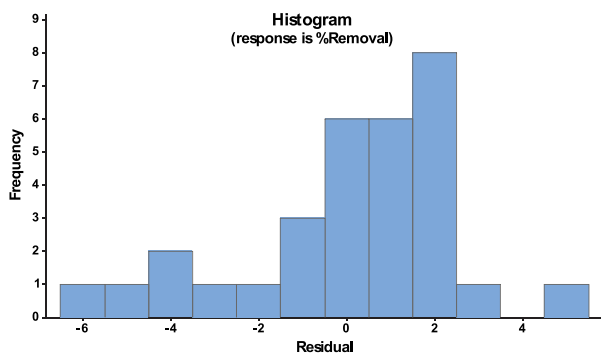


FIG. 4(a). HISTOGRAM OF REGULAR RESIDUAL FOR % REMOVAL VERSUS FREQUENCY

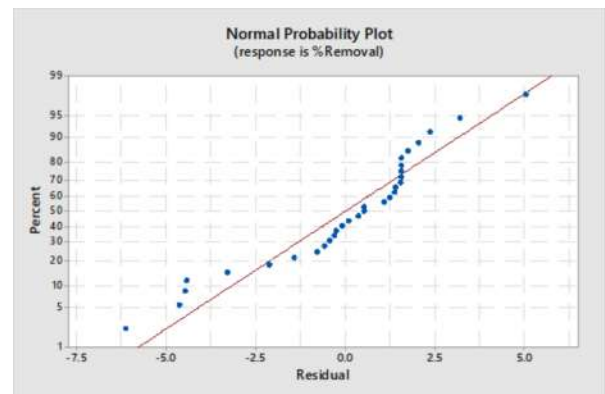


FIG. 4(b). NORMAL PROBABILITY PLOT FOR REGULAR RESIDUAL



FIG. 4(c). THE COMPARISON BETWEEN OBSERVED ORDER AND REGULAR RESIDUAL

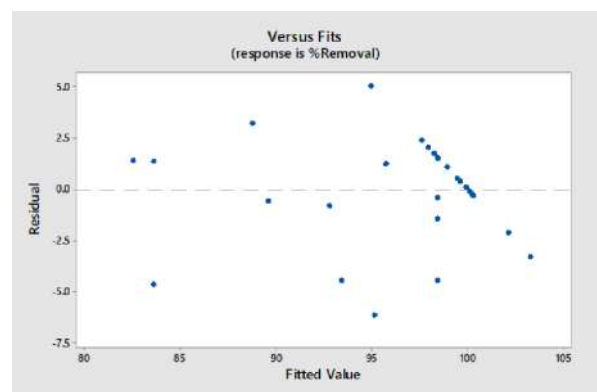


FIG. 4(d). THE RESIDUAL PLOT AGAINST FITTED VALUES

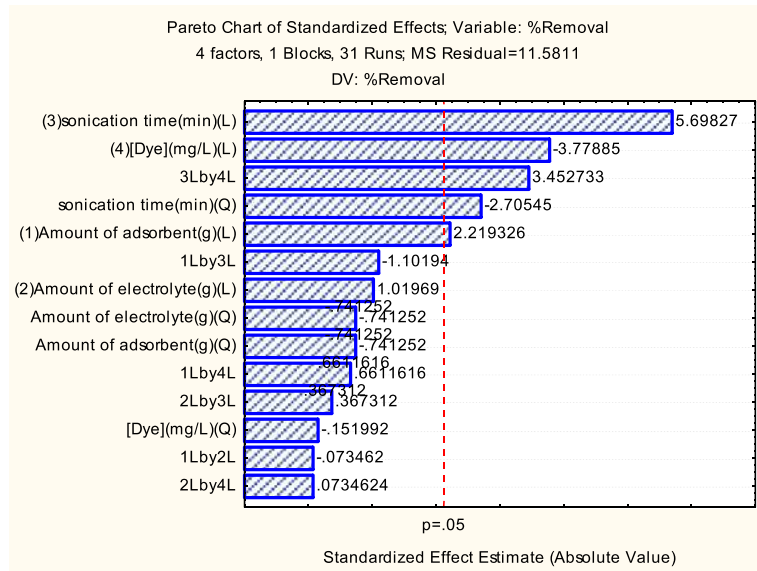


FIG. 5. PARETO CHART OF COEFFICIENTS FOR THE SONO-EC SYSTEM

TABLE 2. MODEL SUMMARY OF EXPERIMENTAL DESIGN OF SONO-EC PROCESS FOR THE REMOVAL OF RR120

S (Root Mean Square Error)	3.403
R <sup>2</sup> (Correlation Coefficient)	82.26%
R <sup>2</sup> (adj)	66.73%
R <sup>2</sup> (pred)	11.16%

TABLE 3. STATISTICAL ANALYSIS OF VARIANCE FOR THE SONO-EC PROCESS

Source	DF	Adj SS	Adj MS	F-Value	P-Value
Model	14	859.1	61.36	5.30	0.001
Linear	4	610.5	152.6	13.18	0.000
A	1	57.04	57.04	4.93	0.041
B	1	12.04	12.04	1.04	0.323
C	1	376.0	376.0	32.47	0.000
D	1	165.3	165.4	14.28	0.002
Square	4	89.71	22.42	1.94	0.153
A*A	1	6.36	6.363	0.55	0.469
B*B	1	6.36	6.363	0.55	0.469
C*C	1	84.77	84.76	7.32	0.016
D*D	1	0.27	0.268	0.02	0.881
2-Way Interaction	6	158.8	26.47	2.29	0.087
A*B	1	0.06	0.062	0.01	0.942
A*C	1	14.06	14.06	1.21	0.287
A*D	1	5.06	5.062	0.44	0.518
B*C	1	1.56	1.562	0.13	0.718
B*D	1	0.06	0.062	0.01	0.942
C*D	1	138.0	138.0	11.92	0.003
Error	16	185.3	11.58		
Lack-of-Fit	10	153.5	15.35	2.91	0.102
Pure Error	6	31.71	5.286		
Total	30	1044			



### 3.3.2 Main Interaction Plots

The simplest graphical tool (Main Effects Plot) is to see, whether the analysis pattern is statistically vital or not. In this plot the response means are plotted against levels of operational parameters. There is no main effect: When factors levels response overlap x-axis (response mean).

In plot Fig. 6 is showing that factors levels significantly moving the target mean values.

### 3.3.3 Full Interaction Plots

The full interaction plot shows response means for the levels of one factor on the x-axis and a separate line for

TABLE 4. THE ESTIMATED PARAMETER AND THEIR IMPLICIT CODED UNITS

Term	Effect	Coef	SE Coef	T-Value	P-Value	VIF
Constant		98.43	1.29	76.52	0.000	
A	3.083	1.542	0.695	2.22	0.041	1.00
B	1.417	0.708	0.695	1.02	0.323	1.00
C	7.917	3.958	0.695	5.70	0.000	1.00
D	-5.250	-2.625	0.695	-3.78	0.002	1.00
A*A	-0.943	-0.472	0.636	-0.74	0.469	1.03
B*B	-0.943	-0.472	0.636	-0.74	0.469	1.03
C*C	-3.443	-1.722	0.636	-2.71	0.016	1.03
D*D	-0.193	-0.097	0.636	-0.15	0.881	1.03
A*B	-0.125	-0.062	0.851	-0.07	0.942	1.00
A*C	-1.875	-0.938	0.851	-1.10	0.287	1.00
A*D	1.125	0.562	0.851	0.66	0.518	1.00
B*C	0.625	0.312	0.851	0.37	0.718	1.00
B*D	0.125	0.062	0.851	0.07	0.942	1.00
C*D	5.875	2.937	0.851	3.45	0.003	1.00

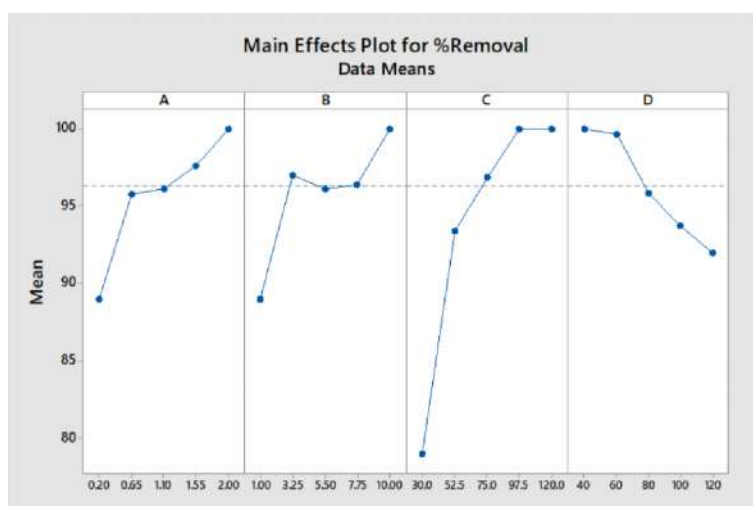


FIG. 6. MAIN EFFECTS PLOT FOR % REMOVAL OF RR120

each level of another factor. If Parallel lines are observed: means that no variation in target response due to amendment in factors levels. If response slope is higher: means additional robust interactions are present among levels of factors for the target response. This plot is reciprocal to ANOVA test. Interaction plot is very useful if there are significant interactions are present among factors for the response values. The lines are not parallel in Fig. 7 for % color removal.

### 3.3.4 Effect of Activated Carbon on Sono-EC Process

Activated carbon has been used to study its effect on the dye removal with sono-electrocoagulation process. Because, it is an excellent adsorbent [28]. Furthermore, on the surface of activated carbon, contaminants are adsorbed. It also reduces toxic nature of  $Cl_2/HOCl/OCl^-$  into non-toxic  $Cl^-$  ions [29]. The Fig. 8(a-b) represent the efficacy of sono-electrocoagulation process regarding the amount of (AC) adsorbent. It is determined by the Response surface graphs (A) that the amount of adsorbent directly proportional to the dye removal potency. From the given Fig. 8(b) represents that mutually the amount of adsorbent and electrolyte considerably affect on the percent removal of the dye. Sonication time and amount of adsorbent also enhanced the percent removal of RR120 dye.

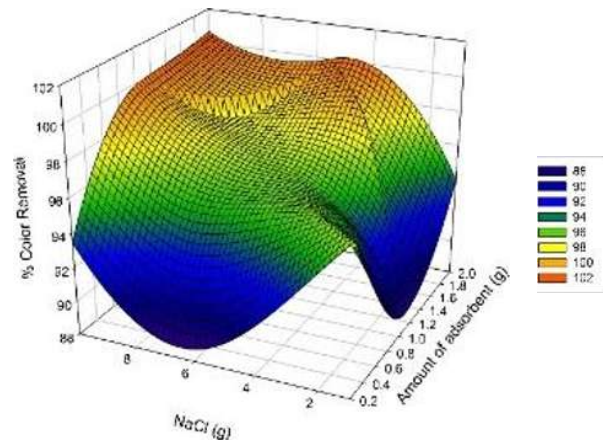


FIG 8(a). AMOUNT OF ADSORBENT (g) AND AMOUNT OF ELECTROLYTE (g)

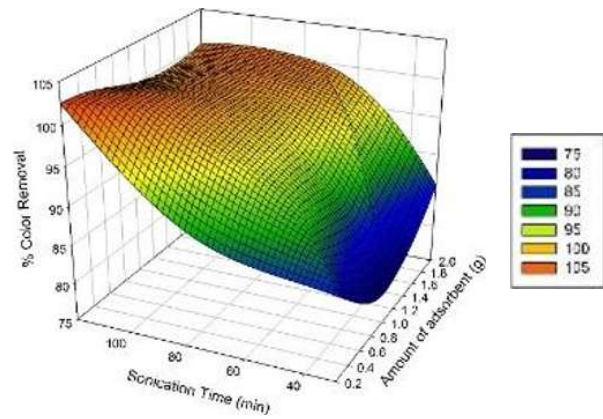


FIG 8(b). AMOUNT OF ADSORBENT (g) AND SONICATION TIME (min)

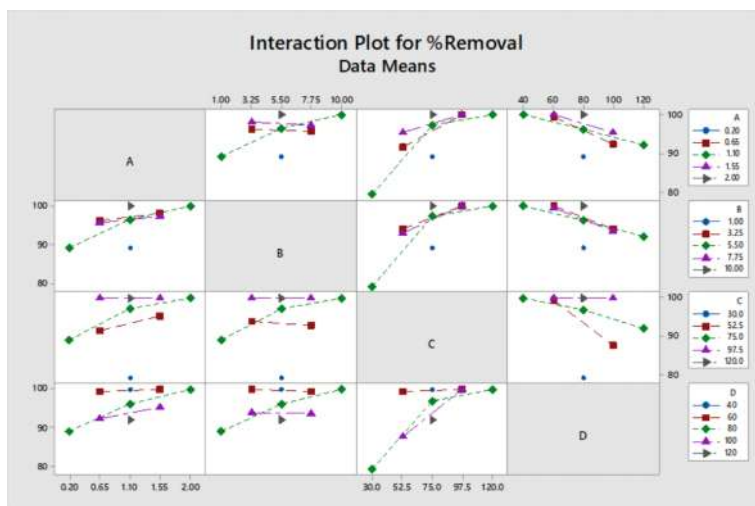
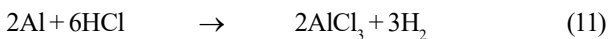


FIG. 7. FULL INTERACTION PLOTS FOR RR120 DYE REMOVAL BY SONO-EC PROCESS

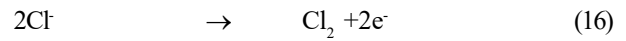
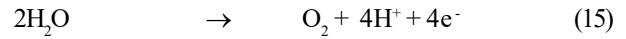
#### 4. EFFECTS OF DIFFERENT OPERATIONAL PARAMETERS ON SONO-EC PROCESS FOR RR120 REMOVAL

##### 4.1 Evaluation of Current Efficiency and Energy Cost

The current efficiency was observed to be (108-154%), with artificial RR120 dye system. This distinction in mass was processed by the corrosion pitting on the surface of aluminium electrode. This mass was mistakenly patterned because of metal surface disintegrated by the following electro-chemical processes.



In aluminum, the observed results are considerably over the expected values for 100% effectiveness process agreed by Faraday's law. This super-faradaic efficiency is due to the aluminum dissolution process, which is compared to the oxidation of the aluminum surface with the synchronous decrease of water to breed hydrogen gas, according to Equation (13) [30]:



The current efficiency is a vital parameter for the EC process as a result of its affects on the time period of the probes. Electrochemically, according to Faraday's law, whenever one Faraday of charge passes through the circuit, about 9.0 g of aluminum is dissolved at anode. On the other hand, the electrochemical side-reactions, the real anode utilization might be diminished or prolonged from this hypothetical respect depending on the wastewater qualities and operational conditions [31].

$$P_{(Watt)} = V I t \quad (19)$$

$$\% \text{ Current Efficiency} = M_o / M_T \times 100 \quad (20)$$

##### 4.2 Influences of Current on Removal Potency

The electric current not only influences on the coagulants formation, additionally, the flocs formation rate, their size and also the flocs chain. To analyze the electric current effect, a series of experiments were performed with 0.2-1.41 A at neutral pH and 4.0 g optimum value of NaCl. The percent removal was improved from 20-60%. The results are showing that the higher current means large population of electrons are available to the electrochemical cell that enhanced the removal potency of dye. However, high generation of current could increase undesirable side-responses like scrounging loss reactions leading to the depletion of hypochlorite concentration [32]. At high current the quantity of metal hydroxide coagulants formation is enhanced. Hence, the rate of removal of pollutants from wastewater is also increased [33].

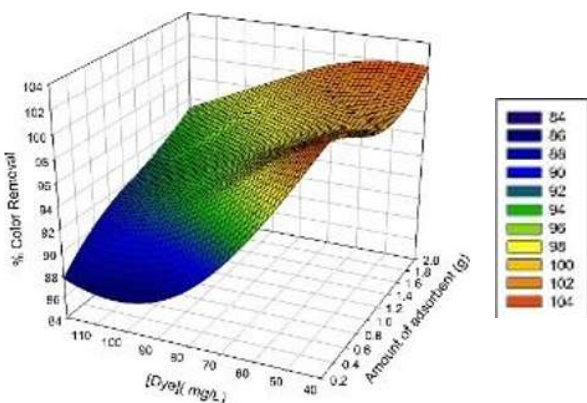


FIG. 8(c). AMOUNT OF ADSORBENT(g) AND DYE CONCENTRATION (mg/L)

### 4.3 Impacts of Quantity of Electrolyte on Removal Efficiency

Conductivity of the wastewater plays an important role to decrease cell's voltage and the energy utilization. It was found by researchers [33-34] that the rate of dye removal enhanced by using NaCl, because of the formation of hypochlorite. The anodic oxidation of chloride ions resulted the chlorine evolutions as shown in Equations (16-17). In water, chlorine rapidly disproportionates and yields hypochloric acid (HClO<sub>4</sub>) and hypochlorite ion (OCl<sup>-</sup>), which can rapidly oxidize organic composites by electrochemical degradation as a

result of indirect oxidation [35]. To study the effect of NaCl concentration on the removal proficiency of the RR120, its amount was varied from 2.0-10.0g. Fig. 10 illustrates that the removal efficiency is depending on the supporting electrolyte dose. The concentration of chloride plays an imperative role in the electro-oxidation process [34-35]. Moreover, it also decreases the passivity of the electrode surface due to its catalytic action [36]. The formation of H<sub>2</sub>O<sub>2</sub>, which is result of the cathodic reaction of atomic oxygen and has been proposed as a supportive compound for dye removal at current of high densities [38].

TABLE 5. EVALUATION OF CURRENT EFFICIENCY AND ENERGY COST

Concentration of RR120 (mg/L)	Current Efficiency (%)	Energy Consumption (KWH/dm <sup>3</sup> )	Cost of Energy (US\$/KWH)	Cost of Electrode (US\$/Kg)	Removal (%)	Current (A)	Amount of NaCl (g)	After Treatment Color of Water
100	154	0.0047	6×10 <sup>-5</sup>	1.18×10 <sup>-3</sup>	100	0.6	4	Colorless
200	112	0.0065	8×10 <sup>-5</sup>	1.71×10 <sup>-3</sup>	100	0.6	4	Colorless
300	108	0.0095	12×10 <sup>-5</sup>	2.42×10 <sup>-3</sup>	100	0.6	4	Colorless
400	116	0.01	13×10 <sup>-5</sup>	2.73×10 <sup>-3</sup>	100	0.6	4	Light Yellow
500	123	0.011	14×10 <sup>-5</sup>	2.44×10 <sup>-3</sup>	100	0.6	4	Dark Yellow

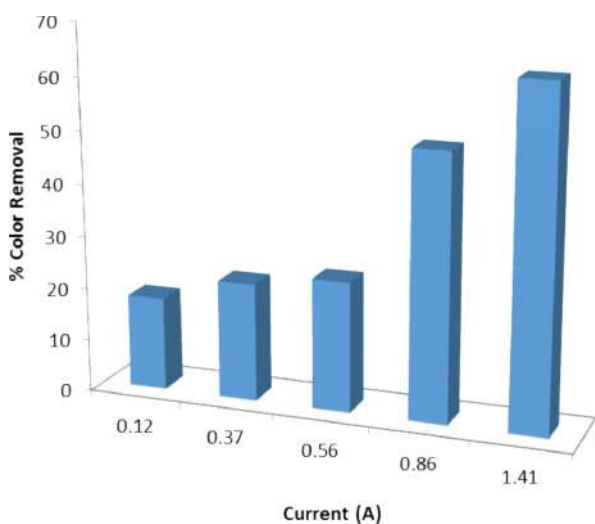


FIG. 9. EFFECT OF CURRENT ON THE % REMOVAL OF RR120 DYE (CO =120 mg/L, SONICATION TIME = 120 min, VOLUME= 1000 mL).

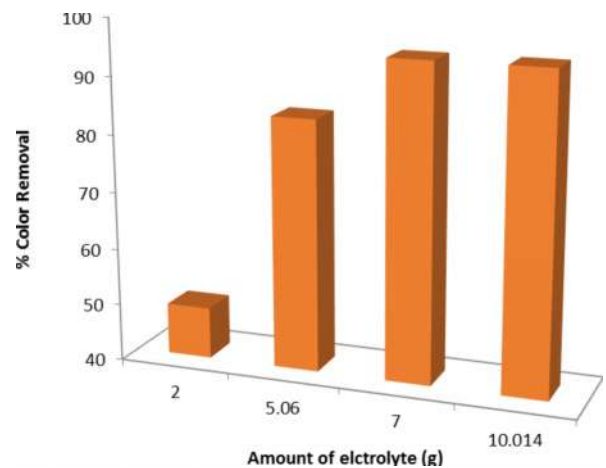


FIG. 10. EFFECT OF AMOUNT OF NAACL ON REMOVAL OF DYE RR120 (120 mg/L), SONICATION TIME = 120 min, VOLUME = 1000 mL)

#### 4.4 Temperature Effect on EC Process

The influence of temperature on the sono-electrocoagulation process was studied at  $30-45^{\circ}\text{C} \pm 0.1^{\circ}\text{C}$ . The results are shown in Fig. 11(a-b), they show that at higher temperatures the removal efficiency is enhanced. Therefore, a linear dependency is observed on the flocculation of dye, since the dye removal follows temperature variations linearly. On the other hand, the dye molecules are discharged into effluent at elevated temperature and reduces the dye removal proficiency. One of the important feature is to be considered that as the temperature increases the rate of diffusion is affected.

The amount of  $\text{Al}(\text{OH})_3 (D_f)$  is determined by the Faraday's law of electrolysis as represented in Equation (21):

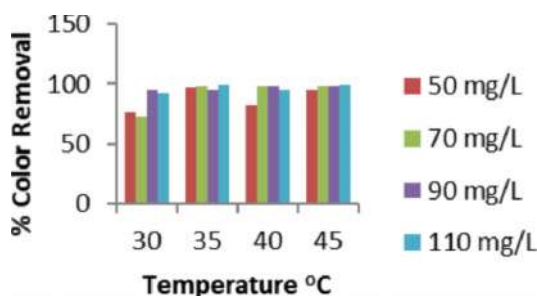


FIG. 11(a). EFFECT OF TEMPERATURE ON % REMOVAL OF DIFFERENT DYE CONCENTRATIONS (mg/L)

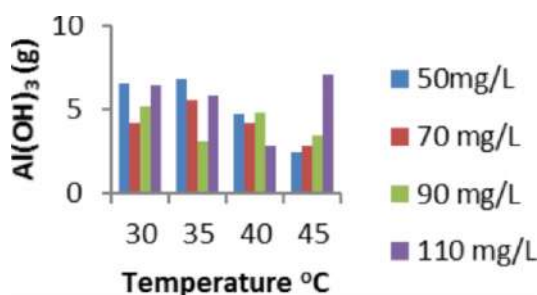


FIG. 11(b). TEMPERATURE EFFECT ON THE AMOUNT OF  $\text{Al}(\text{OH})_3$  FORMATION AT VARIABLE CONCENTRATIONS (mg/L)

$$D_f = I t M / z F \quad (21)$$

where the symbol of the electric current is  $I$ , the unit of current is Ampere (A),  $t$  is the time (s),  $M$  is the atomic mass,  $Z$  is the electron involved, and  $F$  is the Faraday constant (96485.3 C/mol).

#### 5. CONCLUSION

The present work highlighted the remediation of textile industrial pollution. The sono-electrocoagulation process was efficaciously optimized and obtained 100% dye removal from simulated effluent at optimum levels of factors. The optimum values were determined by RSM. The CCD model was significant which was verified from high  $R^2$  (0.8226) value by ANOVA. The effluent of the sono-electrocoagulation treatment possessed properties like palatable, flawless, monochrome and unscented that could be reuse except drinking. After the analysis of data. It was found that the ultrasound irradiation improved the performance of the process in the presence of activated carbon. In the experimental reactor, Aluminium and Carbon electrodes were used successfully for the treatment of simulated discharge. Furthermore, Main and Full interaction plots were also indicated that the corresponding parameters extensively affect on response of the s sono-electrocoagulation process. In the future study, the sono-electrocoagulation process will be applied for the treatment of effluent of SITE Industrial Zone, Karachi, Pakistan.

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